Ammonia Refrigeration 101

DESIGN AND INDUSTRY

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/IAGE COURTESY OF: STELLAR FOOD FOR THOUGHT

Background

- •Joseph Gettemy, PE
 - Graduated ISU 2017
 - Worked for ~5 years as a refrigeration engineer
 - 1.5 years as a field engineer at a pork-processing construction site.
 - Now Mechanical Engineer here at Shive Hattery
 - Focused on Commercial and Industrial projects
 - Pursuing Passive-House certification



AGENDA

- •Intro to Ammonia Refrigeration Why and where?
- •Ammonia Refrigeration as a Sub-Industry
- •Design of Ammonia Systems
- •Ammonia Safety System and Personal
- •Experience as a Refrigeration Engineer.



NH3 REFRIGERANT BY THE NUMBERS

		Halocarbons	Ammonia	CO2	
SAFETY	Recommended Exposure Limit (REL)	1000+ ppm	35 ppm	5000 ppm	
	Upper Operating Pressures	~150 psig	~200-300 psig	~1000 psig	
	COP (Evap 20F, Cond 86F)	5.6 - 6.1	6.3	3.5**	
OPERATION	Initial Cost*	Highest	Lowest	Middle	
	GWP	7-2,500+	0	1	

*Cost given as relative due to fluctuating market costs.

**CO2 is typically most efficient at higher condensing temps

INFORMATION COURTESY OF ASHRAE FUNDAMENTALS HANDBOOK

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Ammonia (NH3) **REFRIGERANT SUMMARY**

- •NH3 as a refrigerant:
 - Negative: Higher Harm Risk Requires more *engineered* safety.
 - Positive: More efficient and less expensive
- •Therefore, NH3 lends itself to larger-scale industrial, especially food production.
 - Greater net benefit from efficiency and cost allows for dedicated safety systems and staff.
 - Results in a singular central system for the whole plant.
- •Other applications include:
 - Server farms
 - Ice Rinks
 - Sustainability applications (due to low GWP)

IMAGE COURTESY OF GOOGLE MAPS

NH3 REFRIG. AS A (SUB)INDUSTRY - CODE

•International Institute of Ammonia Refrigeration (IIAR) standards are typically the governing code.

• IMC defers to IIAR.

•IIAR standards include:

- IIAR 1, Definitions and Terminology.
- IIAR 2, Design of Closed-Circuit Ammonia Refrigeration Systems.
- IIAR 3, Ammonia Refrigeration Valves.
- IIAR 4, Installation of Closed-Circuit Ammonia Refrigeration Systems.
- IIAR 5, Start-up and Commissioning of Closed-Circuit Ammonia Refrigeration Systems.
- IIAR 7, Developing Operating Procedures for Closed-Circuit Ammonia Mechanical Refrigerating Systems.
- IIAR 8, Decommissioning of Closed-Circuit Ammonia Refrigeration Systems.
- IIAR 9, Minimum System Safety Requirements for Existing Closed-circuit Ammonia Refrigeration Systems.



FROM IMC 2021 - CH 11:

1101.1.2 Ammonia refrigerant. 🕑

Refrigeration systems using ammonia as the refrigerant shall comply with IIAR 2, IIAR 3, IIAR 4 and IIAR 5 and shall not be required to comply with this chapter.

IMAGE COURTESY OF: INTERNATIONAL INSTITUTE OF AMMONIA REFRIGERATION

NH3 REFRIG. AS A (SUB)INDUSTRY - CODE

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- IIAR 9, Minimum System Safety Requirements for Existing Closedcircuit Ammonia Refrigeration Systems.
 - IIAR 9 Limited Grandfathering.







NH3 REFRIG. AS A (SUB)INDUSTRY - CODE

- •Systems containing more than 10,000 lbs need a Process Safety Management (PSM) system (per OSHA):
 - Maintained P&IDs
 - Regular documentation and calculation showing compliance
 - Typically, dedicated staff.
- •Updates to these compliance calculations requires frequent engineering visits.

NH3 REFRIG. AS A (SUB)INDUSTRY - NUANCE

- •For Engineers, these visits create frequent repeat customers and relationship building.
- •Because the system is a singular central design, changes to a portion of the system require knowledge of the whole system.



IMAGE COURTESY OF: PROGRESSIVE AE





SYSTEM DESIGN - BASICS

•Ammonia refrigeration operates using the refrigeration cycle.



SYSTEM DESIGN

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FLUID SATURATION

- •Refresher: *at a given* liquid and vapor
 - At temp: saturated

pressure and temperature: fluid transitions between Above temp: <u>super-heated</u>

• Below temp: sub-cooled



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FLUID SATURATION

		Refrigerant 717 (Ammonia) Properties of Saturated Liquid and Saturated Vapor													
		Temp.,* Pressure,	Density, lb/ft ³	Volume, Enthalpy, ft ³ /lb Btu/lb-°F		Entropy, Btu/lb-°F		Specific Heat c _p Btu/lb-°F		C _p /C _v	Thermal Conductivity Btu/hr-ft-°F		Temp.,*		
		г	psia	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Liquid	Vapor	Vapor	Liquid	Vapor	г
	ľ	25.00	53.720	40.20	5.3307	70.072	618.974	0.1547	1.28726	1.0983	0.6271	1.3894	0.3302	0.01331	25.00
		30.00	59.730	39.96	4.8213	75.585	620.305	0.1660	1.27842	1.1019	0.6366	1.3951	0.3253	0.01345	30.00
EVAP	l	35.00	66.255	39.72	4.3695	81.116	621.582	0.1772	1.26975	1.1056	0.6465	1.4012	0.3204	0.01360	35.00
\rightarrow	•	40.00	73.322	39.48	3.9680	86.666	622.803	0.1883	1.26125	1.1094	0.6569	1.4078	0.3155	0.01376	40.00
		45.00	80.962	39.24	3.6102	92.237	623.967	0.1993	1.25291	1.1134	0.6678	1.4147	0.3107	0.01392	45.00
	ł			L		ļ	L					ļ	<u> </u>		<u> </u>
	II	75.00	140.590	37.73	2.1217	126.126	629.647	0.2640	1.20570	1.1410	0.7440	1.4670	0.2825	0.01504	75.00
COND		80.00	153.130	37.47	1.9521	131.861	630.359	0.2745	1.19823	1.1470	0.7580	1.4780	0.2780	0.01525	80.00
	• [[85.00	166.510	37.21	1.7983	137.624	630.999	0.2850	1.19085	1.1530	0.7740	1.4900	0.2734	0.01548	85.00
		90.00	180.760	36.94	1.6588	143.417	631.564	0.2955	1.18356	1.1590	0.7900	1.5020	0.2689	0.01571	90.00
		95.00	195.910	36.67	1.5319	149.241	632.052	0.3059	1.17634	1.1660	0.8070	1.5150	0.2644	0.01595	95.00
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SYSTEM DESIGN

•Ammonia refrigeration operates using the refrigeration cycle.

•Comparable to a VRF system (cooling only)



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SYSTEM DESIGN - SCALE















SYSTEM DESIGN - SCALE





EVAPORATOR











•Most basic system.

•Functions when required temperatures are similar.





•Allows for two temperature

• Usually refrigerated and below-

Booster compressor

• 3rd pressure/temperature.



•In intercooler:

1. Superheated vapor from compressor enters vessel.

2. Vessel is at saturation with both liquid and vapor.

3. Superheated vapor cools to saturation and converts some of the sat liquid to vapor also.

4. Vessel is maintained with sufficient liquid to keep temp and pressure at saturation.



• Evaporator coil size limited.

• If too large, liquid may evaporate before filling coil.

•Frequent issue with lower temps and heat-exchangers.

SYSTEM DESIGN – FLOODED – TWO STAGE



SYSTEM DESIGN – FLOODED – TWO STAGE



•Adds surge drums above evaporator/ heat-exchanger.

contains liquid and fills coils $\sim 2/3$ full.

SYSTEM DESIGN – FLOODED – TWO STAGE



• Increases lbs ammonia

SYSTEM DESIGN – RECIRCULATED – TWO STAGE

SYSTEM DESIGN – RECIRCULATED – TWO STAGE

EVAP EVAP EVAP include: HPR - HIGH PRESSURE RECIEVER COND • Electric • Hot gas LIQUID COMP EVAP EVAP EVAP SUCTION INT -INTERCOOLER LIQUID COMP SUCTION

SYSTEM DESIGN – DEFROST

- •Coils will accumulate ice and require defrost. Methods
 - Air (if above freezing)

SYSTEM DESIGN – DEFROST – HOT GAS

Most common defrost.

 Hot gas from compressor discharge heat coils:

Higher temp: three-pipe
Defrost gas returns through suction.

Lower temp: four-pipe.
Defrost liq/gas returns through separate line to high-stage suction.

OTHER DESIGN – THERMOSYPHON OIL COOLING

- •Screw compressors inject oil (lubricant) with ammonia before compression.
- •Oil is then separated in vessel below.
- •To cool oil:
 - Vessel is suspended above compressors.
 - Liquid ammonia gravity-fed to ammonia-oil HEX at compressor.
 - Liquid converts to vapor as it cools oil.
 - Vapor returns to vessel.

OTHER DESIGN – UNDERFLOOR WARMING AND MOISTURE MANAGEMENT

- •Hot gas from compressors exchanges heat with glycol.
- •Glycol runs under slab to prevent ice.
- •Insulation and pipe integrity is (ideally) regularly inspected.
- •As needed, additional moisture-management practices are used:
 - Local exhaust
 - Localized fans
 - Dehumidification

regularly inspected. ement practices are

OTHER DESIGN – SKIDS

•Shop made skids - for quick install and cost savings.

- Either as a central machine room OR
- Distributed system (mini-machine rooms)

•Mini-machine-room skids serve separate parts of facility:

- Refrigerant reduction.
- Quick install.
- Loss of redundancy.

SYSTEM DESIGN - SAFETY

- •Detection and Alarm PPM Limits:
 - 25 ppm Alarms
 - 150 ppm Emergency Ventilation
 - Often Emergency Ventilation will start sooner
 - 40,000 ppm System shutdown
 - For flamability
- •Emergency ventilation Low Louvers to High Upblast Exhaust Fans
 - Sweep the room

SYSTEM DESIGN - SAFETY

- •EPCS Emergency Pressure Control System releases pressure from higher-pressure to lower.
- Pressure Relief System Releases pressure to the atmosphere at max vessel pressure.
 - These relief valves are tied together in a relief tree, which must be engineered for compliance.
 - Requires iterative calculation and typically software or a spreadsheet macro.

Personal Safety

- •Use your nose Ammonia detectable as low as ~5ppm.
- •Ammonia is invisible but will create a cloud during a larger leak.
- •When encountering a leak:
 - Stay calm and walk
 - Get low Ammonia rises
 - When outside Look for wind direction.
 - Windsocks are required at an ammonia site.

•Buddy-system when entering a cooler, freezer, or other unoccupied territory.

Being a Refrigeration Engineer

- •My own experience:
 - 15 months as a field engineer Pork plant start to finish.
 - Remaining time as safety-systems engineer.
- •Pros and Cons often the same:
 - Multi-day site visits ~1-3 times/month coast to coast.
 - Deep knowledge of a specific field subject matter expert fast.
 - Very engineering-focused, minimal interaction with other disciplines.

